

## CONSERVATION OF MASS

RECAP: General conservation law for "B" with density  $b$

$$\frac{D}{Dt} \int_{\Omega} b d\Omega = \int_{\Omega} q^B d\Omega + \int_{\partial A} T_{\dots j}^B n_j dA \quad \dots \text{ integral form}$$

$$\frac{\partial b}{\partial t} + \frac{\partial}{\partial x_j} (b u_j) = q^B + \frac{\partial}{\partial x_j} T_{\dots j}^B \quad \dots \text{ differential form}$$

In this video,  $B = \text{mass}$ .

$$b = \rho = \text{mass density}$$

$$q^B \equiv 0 \iff \text{no volumetric generation of mass possible}$$

$$T_{\dots j}^B = 0 \iff \text{no net exchange of mass on a Lagrangian boundary}$$

$q^B =$  volumetric source of B  
 $T_{\dots j}^B =$  surface exchange rate of B on a Lagrangian boundary

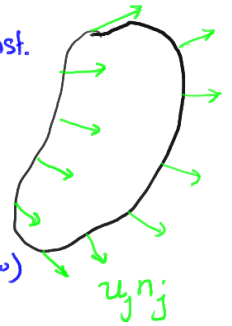
INTEGRAL FORM For an arbitrary Lagrangian volume  $\Omega$

Conservative Lagrangian form:  $\frac{D}{Dt} \int_{\Omega} \rho d\Omega = 0 \Rightarrow M = \int_{\Omega} \rho d\Omega = \text{const.}$

Conservative Eulerian form:  $\int_{\Omega} \left[ \frac{\partial \rho}{\partial t} + \frac{\partial}{\partial x_j} (\rho u_j) \right] d\Omega = 0$

$\rho u_j =$  convective flux of mass (mass carried by the flow)

$\rho u_j n_j = \rho \underline{u} \cdot \hat{n} =$  mass crossing a unit surface with normal  $\hat{n}$ .



Applying divergence theorem:  $\int_{\Omega} \left[ \frac{\partial \rho}{\partial t} + \frac{\partial}{\partial x_j} (\rho u_j) \right] d\Omega = 0$

Differential forms

Conservative:  $\frac{\partial \rho}{\partial t} + \underbrace{\nabla \cdot (\rho \underline{u})}_{\text{rate of depletion of mass by the flow per unit volume of an infinitesimal volume}} = 0$  OR  $\frac{\partial \rho}{\partial t} + \underbrace{\frac{\partial (\rho u_j)}{\partial x_j}}_{\text{rate of depletion of mass by the flow per unit volume of an infinitesimal volume}} = 0.$

Lagrangian:  $\frac{1}{\rho} \frac{D\rho}{Dt} = -\nabla \cdot \underline{u} = -\frac{1}{V} \frac{DV}{Dt}$

$$V \frac{D\rho}{Dt} + \rho \frac{DV}{Dt} = 0$$

$$\boxed{\frac{D(\rho V)}{Dt} = 0}$$

Aside:  $\frac{\partial \rho}{\partial t} + \underline{u} \cdot \nabla \rho + \rho \nabla \cdot \underline{u} = 0$

$$\frac{D\rho}{Dt} + \rho \nabla \cdot \underline{u} = 0.$$

Incompressible fluid:  $\boxed{\nabla \cdot \underline{u} = 0}$  OR  $\frac{D\rho}{Dt} = 0.$  (Incompressible flow)

(constant density)

